



## Study of instability driven mixing via improved tracking and transport control

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### **Outline of the talk**

- 1. PDE, conservation law, and discontinuity
- 2. Improving the front tracking method
- 3. Comparison and benchmarks
- 4. Comparison of Rayleigh-Taylor instability
- 5. Transport control with tracking
- 6. Conclusion
- 7. Application to other scientific and engineering problems



## PDE

- Hyperbolic equation (wave equation)
- Parabolic equation (diffusion equation)
- Elliptic equation (steady state equation)



# **Parabolic equations**

In 1-D: 
$$\frac{\partial u}{\partial t} = D \frac{\partial^2 u}{\partial x^2}$$
 or  $u_t = D u_{xx}$ 

In multi-dimension:  $u_t = D\Delta u$ 

where 
$$\Delta = \sum_{i=1}^{d} \frac{\partial^2}{\partial x_i^2}$$
 is the Laplace operator

Parabolic equation flattens all variation (variation deminishing.

Physically, it is the diffusion equation originated from the heat transfer equation.



## Solution in infinite space

Initial condition:  $u(x,0) = \varphi(x)$ Solution in infinite domain  $(-\infty, \infty)$ 

$$u(x,t) = \frac{1}{\sqrt{4\pi Dt}} \int_{-\infty}^{\infty} e^{-\frac{(x-y)^2}{4Dt}} \varphi(y) dy$$

1. Singularity:  $\varphi(x) = \delta(x)$ 

2. Discontinuity: 
$$\varphi(x) = h(x)$$

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# Singular initial condition

$$\varphi(x) = \delta(x) = \begin{cases} \infty & x = 0\\ 0 & x \neq 0 \end{cases}$$

$$u(x,t) = \frac{1}{\sqrt{4\pi Dt}} e^{-\frac{x^2}{4Dt}}$$







### Discontinuous initial condition

$$\varphi(x) = h(x) = \begin{cases} 1 & x \le 0\\ 0 & x > 0 \end{cases}$$









## Hyperbolic equation

1-D wave equation:

$$u_{tt} - a^2 u_{xx} = 0 \qquad \Rightarrow \qquad u_t + a u_x = 0 \qquad u_t - a u_x = 0$$

Traveling wave solution:

$$u(x,t) = \varphi(x-at) \quad u(x,t) = \psi(x+at)$$

Characteristics, along the curve

$$\frac{dx}{dt} = a, \quad \frac{du}{dt} = 0$$



## Linear and nonlinear equations

Linear equation: a = a(x, t)

Typical equation:  $u_t + au_x = 0$  a = const

Nonlinear equation: a = a(x, t, u)

Typical equation (Burgers equation)

$$u_t + uu_x = 0, \quad a = u$$

Conservation law:

$$u_t + f(u)_x = 0, \quad a = f'(u)$$



- 1. Shock is a result of the intersection of characteristics.
- 2. Shock is a discontinuity across which physics change sharply.
- 3. Shock speed is derived from conservation—Rankine-Hugoniot condition

s[u] = [f(u)]

 $[u] = u_R - u_L \quad [f(u)] = f(u_R) - f(u_L)$ 

s is the shock speed.



# Examples of conservation law

- 1. Traffic Flow in a highway
- 2. Flood wave
- 3. Glaciers motion
- 4. Chemical exchange process
- 5. Oil reservoir
- 6. Gas dynamics



## **Traffic flow**

$$\rho_t + Q(\rho)_x = 0$$

Greenberg (1959) studied the traffic of Lincoln Tunnel and found:

$$Q(\rho) = a\rho \log \frac{\rho_j}{\rho}$$
$$a = 17.2(mph), \quad \rho_j = 228(vpm)$$

Traffic relaxation:

$$\rho - \rho_0 \propto \sqrt{\frac{1}{t}}$$



## Flood wave

$$\frac{\partial A}{\partial t} + \frac{\partial Q}{\partial t} = 0$$

A: The cross sectional area of the river bed *Q*: Water flux in volume

Kleitz (1858) and Seddon (1900) used balance Between gravitational force and friction force derived:

$$Q = vA = \sqrt{\frac{A^3 g \sin \alpha}{PC_f}} \propto A^{3/2}$$



## Equation for gas dynamics

Mass, momentum and energy conservation:

$$\rho_t + (\rho u)_x = 0$$
$$(\rho u)_t + (\rho u^2 + P)_x = 0$$
$$e_t + (u(e+P))_x = 0$$

Equation of state (EOS):

 $P = P(\rho, e)$ 



# **Riemann problem**

$$U(x,0) = \begin{cases} U_L & x < 0\\ U_R & x > 0 \end{cases}$$
  
1. Initial Condition:  
$$U_L = \begin{pmatrix} \rho_L \\ u_L \\ p_L \end{pmatrix} \quad U_R = \begin{pmatrix} \rho_R \\ u_R \\ p_R \end{pmatrix}$$
  
2. Invariance of solution: 
$$U(x,t) = V\left(\frac{x}{t}\right)$$

3. Four states:  $U_L$ ,  $U_L^*$ ,  $U_R^*$ ,  $U_R$ 

4. Three waves: left wave, contact, right wave.



# Glimm Scheme

Given states at the *n*th time step:  $U_j^n$ Glimm's scheme advances the state via:

$$U_{j+1/2}^{n+1/2} = V\left(\frac{\xi}{t^{n+1/2}}\right), \quad \xi = (j+1/2)h + \mathcal{H}$$
$$U_{j}^{n+1} = V\left(\frac{\zeta}{t^{n+1}}\right), \qquad \zeta = jh + \mathcal{H}$$
$$\mathcal{G} \text{ is a random variable in } \left[-\frac{1}{2}, \frac{1}{2}\right]$$

The convergence of Glimm scheme is through large Number theorem and is the first significant convergence Proof for the gas dynamics equations.



## Godunov scheme

$$\frac{U_{j}^{n+1} - U_{j}^{n}}{\Delta t} + \frac{f_{j+1/2} - f_{j-1/2}}{\Delta x} = 0$$
  
$$f_{j+1/2} = f(V(x_{j+1/2} / t_{n+1/2}))$$



#### **The Discrete Representation of The Front Tracking**



A 2D Representation

A 3D Interface



# The 3D interface



"Three Dimensional Front Tracking", J. Glimm, J. Grove, X. L. Li, K. Shyue, Y. Zeng and Q. Zhang, SIAM J. Sci. Comp., 19, 1998.



### Front Tracking Method

• Front tracking method is implemented in code *FronTier*.



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#### Major components:

- 1. A moving mesh to represent interface
- 2. Navier-Stokes equations
- 3. Dynamic subgrid scale models

#### Procedure to solve:

- 1. Propagate points on interface
- 2. Redistribute surface mesh
- 3. Reconstruct the tangled part in surface mesh
- 4. Solve equations for liquid and gas separately with ghost fluid method

#### Numerical methods related to front tracking:

- 1. Coupling fluid solver with interface propagation
- 2. Handling topological changes

### Ghost Fluid Method

- The ghost states on the other side of the interface is constructed by a ghost fluid method (B.Khoo *et.al.* 2005).
- Stencil across the interface
- Solving a Riemann problem
- Using the middle states from the Riemann problem to construct the ghost states
- Surface tension force is modeled in the Riemann problem by

$$p_l^* - p_r^* = \sigma \kappa$$

 $s_4$  $s_1$  $s_3$  $s_5$  $s_2$  $\mathbf{s}$  $s_3$  $s_2$  $s_1$  $s_5$  $s_{lg}$  $s_{lg}$  $s_3$  $s_1$  $s_2$  $s_3 = (\rho_l, u_l, p_l) \ s_l^* = (\rho_l^*, u_l^*, p_l^*)$  $s_{lq} = (\rho_l, u_l^*, p_l^*)$ 

- 2D and 3D
  - Project interface normal vectors onto cell centers.
  - Construct ghost states along normal directions.

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### **Interface Point Propagation**

Interface states are reconstructed from the interpolation of real and ghost states



Advantage: No need to solve Navier-Stokes equations on the interface. More robust and efficient than our previous front tracking method.



# **Geometry and Topology**

- The challenge to Lagrangian method
- Eulerian level set method
- The Marching cube method
- Reverse engineering: grid-based tracking
- Combining the best of Lagrange and Euler
- The locally grid-based tracking method



# Level Set Methods

- A popular and powerful scheme for interface tracking is to compute the interface position by propagating a function whose level set corresponds to the interface position •
  - The interface location at time t is given by  $\phi(\mathbf{x},t) = 0$  where

 $\phi_t + F \left| \nabla \phi \right| = 0$ 











- See the books of Sethian: "Level Set Methods and Fast Marching Methods" or Osher and Fedkiw: "Level set methods and dynamic implicit surfaces" Designed to handle interface topology changes automatically However interface are limited to shapes that can be represented by level sets ouples to a numerical scheme for updating flows states on a volume esh via a ghost fluid (extrapolation across interfaces) method
- Vhen fully developed has similar features to explicit interface methods n many aspects



## The idea of grid-based





# **Grid-based Front Tracking**

- 1. The common agreement: interface is greatly simplified in Eulerian grid.
- Marching Cubes, Lorenson and Cline, 1987, (Static, Computer Graphics).
- 3. Level set method, Osher and Sethian, 1988, (Implicit).
- 4. Grid-based front tracking, SJSC, 21, 6 2000, (Explicit and Dynamic).







## **Grid-based topological correction**









#### Interface bifurcation under grid-based front tracking method



"Robust Computational Algorithm for Dynamic Interface Tracking in Three dimensions", J. Glimm, J. Grove, X. L. Li and D. C. Tan, SIAM J. Sci. Comp., 21, 2000.



#### **Basic FronTier Test Simulations**



Case Bifure-1



#### **Interface Topological Changes**

- Grid based tracking is robust but too diffusive.
- Challenge: Robustness of the algorithm is crucial for large scale computing.



#### Grid based tracking

Grid free tracking



#### **Interface Topological Changes**

- Algorithms to handle topological changes
  - Grid free tracking (GF)
  - Grid based tracking (GB)
  - Locally grid based tracking (LGB)



#### **Robust Locally Grid Based (LGB) Untangle**

 A robust algorithm to reconnect a grid based surface mesh with a grid free surface mesh



- Advantage
  - Local, it is suitable for large scale computing.
  - Robust, It generates topologically valid surface mesh.

"A Simple Package for Front Tracking", J. Du, B. Fix, J. Glimm. X. L. Li, Y. Li, L. Wu, JCP, 213, 2006.


### **Benchmark Plus**





### 3D rotation of slotted sphere





## Fifth order level set (WENO) vs. fourth order front tracking (Runge-Kutta)





## Front tracking reversal test of interface in the deformation velocity field



Figure 2: Reversal test of a 2D interface in the deformation velocity field. The computation is performed in a  $128^2$  computational mesh. In comparison with Rider and Kothe (95), the resolution of the interface matches the best results by the Marker Particle methods.



#### **Resolution Test**





## Front tracking reversal test of interface in 3D deformation velocity field





## Topological bifurcation: it's done!





#### Topological merging of 3D surface mesh



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#### Examples

Interface bifurcation and merging are commonly observed in multiphase flow





mesh bifurcation in a curvature dependent surface propagation

mesh merging in a droplet collision simulation



## **Conservative Front Tracking**



#### The extended stencil method





$$u_{j}^{n+1} = u_{j}^{n} - \frac{\Delta t}{\Delta x} \left( F_{j+1/2}^{L} - F_{j-1/2} \right)$$

$$u_{j+1}^{n+1} = u_{j+1}^{n} - \frac{\Delta t}{\Delta x} \left( F_{j+3/2} - F_{j+1/2}^{R} \right)$$

$$F_{j+1/2}^{L} = F \left( u_{j-1}^{n}, u_{j}^{n}, \overline{u}_{j+1}^{n}, \overline{u}_{j+2}^{n} \right)$$

$$F_{j+1/2}^{R} = F \left( \overline{u}_{j-1}^{n}, \overline{u}_{j}^{n}, u_{j+1}^{n}, u_{j+2}^{n} \right)$$

$$F_{j+1/2}^{L} \neq F_{j+1/2}^{R}$$





#### 1. Chern and Colella, LLNL Report, 1987

#### 2. D. K. Mao, JCP, 1991, 1993

3. Pember, JCP, 1995



Neglect higher order term and note that  $\int_{\Delta V} u dV = \int_{S_M} u v_n dS \Delta t$ 

We have the integral form of conservation

$$\frac{\partial}{\partial t} \int_{V} u dV - \int_{S_{M}} u v_{n} dS + \oint_{S} F_{n}(u) dS = 0$$

This can also be written as

$$\frac{\partial}{\partial t} \int_{V} u dV + \int_{S_{F}} F_{n}(u) + \int_{S_{M}} (F_{n}(u) - v_{n}u) dS = 0$$

Or simply

$$\frac{\partial}{\partial t} \int_{V} u dV + \oint_{S} (F_n(u) - v_n u) dS = 0$$

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### **Conservative Interface-Interior Coupling**

The conservation law:

$$u_t + f(u)_x = 0$$

The Rankine-Hugoniot condition:

$$f(u_L) - su_L = f(u_R) - su_R$$



In 1-D, this lead to:

$$\Delta x_{j}^{n+1} U_{j}^{n+1} = \Delta x_{j}^{n} U_{j}^{n} - \Delta t \left( F_{I}^{n+1/2,L} - F_{j-1/2}^{n+1/2} \right)$$
$$\Delta x_{j+1}^{n+1} U_{j+1}^{n+1} = \Delta x_{j+1}^{n} U_{j+1}^{n} - \Delta t \left( F_{j+3/2}^{n+1/2} - F_{I}^{n+1/2,R} \right)$$

where

$$F_{I}^{n+1/2,L} = f(u_{L}^{n+1/2}) - s^{n+1/2} u_{L}^{n+1/2}$$

$$F_{I}^{n+1/2,R} = f(u_{R}^{n+1/2}) - s^{n+1/2} u_{R}^{n+1/2}$$

$$F_{I}^{n+1/2,L} = F_{I}^{n+1/2,R}$$

Due to Rankine-Hugoniot condition



### 1D Conservative Front Tracking Geometry

#### Two cases

- Fronts do not cross the cell center in one time step.
- Fronts do cross the cell center in one time step.



Case 1

Case 2

New cell average  $v_i^n$  and  $v_{i+1}^n$ :

$$v_i^n = \frac{1}{(\sigma(t_n) - x_{i-1/2})} \int_{x_{i-1/2}}^{\sigma(t_n)} U(x, t_n) dx$$

$$v_{i+1}^{n} = \frac{1}{(x_{i+3/2} - \sigma(t_n))} \int_{\sigma(t_n)}^{x_{i+3/2}} U(x, t_n) dx$$

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#### **Convergence test of conservative tracking**

n (mesh)	shock position error	order	error L1	order
50	4.8e-2		0.481530	
100	1.3e-4	8.5	0.034279	3.8
200	4.3e-5	1.6	0.013060	1.4
400	1.6e-6	1.4	0.004242	1.6



In multi-dimensional case, we consider the time space equation:

$$\vec{F} = u\hat{n}_t + f(u)\hat{n}_x + g(u)\hat{n}_y + h(u)\hat{n}_z \qquad \nabla \cdot \vec{F} = 0$$
  
On a time-space cell  
$$\oint_{TS} \vec{F} \cdot \hat{n}_{ts} dS_{ts} = 0$$

Cell-merge is needed if the volume of the time-space cell is less than half of the regular cell, in 2-D the time space cell is constructed the same way as the 3-D grid based interface.





The time-space interface between n and n+1 time steps





Before cell merger





After cell merger



	Conservative	Nonconsertive
	Tracking	Tracking
Mass		
Error	0.0	0.21%
X-Mom		
Error	0.0	0.21%
Energy		
Error	0.0	0.21%









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## **Rayleigh-Taylor Instability**





## Inertial Confinement Fusion (ICF)





### FronTier application: chaotic mixing







### FronTier application: chaotic mixing



Chaotic mixing is not only important to ICF, but also a test of large scale FronTier application to petascale computing. We have implemented a load balanced parallel algorithm and ran up to 1024 processors on New York Blue. Collaboration with B. Cheng, John Grove, and D. Sharp at LANL.







## **Acceleration Driven Mixing**

• Rayleigh-Taylor (RT), steady acceleration:

$$h = \alpha Agt^2; A = \frac{\rho_2 - \rho_1}{\rho_2 + \rho_1}$$



## The $\alpha$ Paradox

 $h_{h} = \alpha Agt^{2}$ 

# David Youngs and K.Read (1984)



## Read's Experiment (1984)

3D alcohol/air	Exp # 29	Alpha = 0.073
	39	0.076
	58	0.077
3D NaI soln./Pentane	e Exp # 33	Alpha = 0.066
	35	0.071
3D NaI soln./Hexane	Exp # 62	Alpha = $0.063$
	60	0.073



#### **Summary of Experiments**

Experiments						
Read/Youngs	'84	$\alpha_b \sim 0.58 - 0.65$	2D			
		$\alpha_b \sim 0.063 - 0.077$	3D			
Kucherenko	'91	$\alpha_b \sim 0.07$	3D			
Snider/Andrews	'94	$\alpha_b \sim 0.07 \pm 0.007$	3D			
Schneider/Dimonte/Remington	'99	$\alpha_b \ge 0.054$	3D			
Dimonte/Schneider	'99	$\alpha_b \sim 0.05 \pm 0.01$	3D			



#### The Alpha of Bubbles





#### **FronTier TVD**



#### Agt = 25.3 h = 4.16 Density plot




(a) (b) (c)  
$$M_1 = \frac{4\pi}{3} r^3 \rho_L \qquad M_2 = \frac{4\pi}{3} \rho_L + \frac{4\pi}{3} (R^3 - r^3) \rho_H$$

$$f_1 = f_2 = \frac{4\pi r^3}{3} (\rho_H - \rho_L) g$$

$$a_1 = \frac{\rho_H - \rho_L}{\rho_L} g \qquad a_2 = \frac{\rho_H - \rho_L}{\rho_L + \left(\frac{R^3}{r^3} - 1\right)\rho_H} g$$



# Goal of mixing study

- Predict large scale features. Size of mixing zone
- Predict statistics (means, variances) of fluid quantities
- For use in combustion
  - Predict full probability distribution (PDF) of species concentration and temperatures
- Accurate models down to atomic level of mix are needed
- These must be sensitive to transport, Reynolds number, Schmidt number



Real vs. Ideal Mixing Physical vs. Numerical Scale Breaking

- Numerical nonideal effects
  - Numerical surface tension
  - Numerical mass diffusion
- Physically nonideal effects
  - Surface tension
    - Surfactants, variable surface tension, Marangoli force
  - Mass diffusion
    - Initial or for all times
  - Viscosity
  - Compressibility
  - Long wave length initial perturbations



# Main New Results

- Systematic agreement of simulation with experiment and theory
- Alpha, bubble width, bubble height fluctuations
  - Most relevant experiments included in agreement
    - Reed-Youngs, Smeeton-Youngs, Andrews experiments
    - Omitted:
      - Immiscible with surfactant (Dimonte and Smeeton-Youngs)
      - Initial diffusion layer (in progress)
      - Subgrid models
      - Nonideal initial conditions

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## Scale Breaking: Experiments and Simulations

Scale breaking physics	Alpha- experimental	Alpha- simulation	Experiment s	Fluids
Surface tension	0.050-0.077	0.067	RY, SY	Liquid/liquid; liquid/gas
Surface tension with surfactant	0.050-0.061	????	SY,DS	Liquid/liquid
Mass diffusion	0.070	0.069	BA	Gas/gas
Initial mass diffusion	0.062	????	SY	Liquid/liquid
Viscosity	0.070	????	SA	Liquid/liquid
Compressibility		Up to 0.2	Lasers	plasmas



## Comparison of Mixing Rates: Comparison, Simulation and Theory

	Theory	Experiment	Simulation
height	0.06	0.067	0.062
radius	0.01	0.01	0.01
fluctuations in height		0.028	0.034



# **Turbulent Mixing**

- Acceleration driven mixing
  - Steady acceleration Rayleigh-Taylor mixing
  - Impulsive acceleration Richtmyer-Meshkov mixing
- Most RT computations underpredict mixing rates relative to experiments
  - Simulation analysis using time dependent densities (Atwood number) makes this point
- Cause appears to be numerical mass diffusion, which reduces the local density contrast and thus the large scale mixing rates
  - Numerical surface tension also significant
- Questions raised about the role of initial noise in the experiments



## Numerical Non-Ideal Effects

- Numerical mass diffusion
  - Removed by tracking
  - Errors modify density contrast by a factor of 2 for typical grids
- Numerical surface tension
  - Reduced by local grid based (LGB) tracking
  - Errors proportional to curvature x Delta x
  - Arises from approximation of interface by a line segment within each mesh block
  - Arises from grid level description of interface and thus occurs for all untracked methods



# **Time Dependent Atwood Number**

- Atwood number
  - For each z  $A = \frac{1}{\rho_2 + \rho_2}$

$$A = \frac{\rho_2 - \rho_1}{\rho_2 + \rho_1}$$

- Compute the maximum and minimum density

- Form a space (height) and time dependent A(z,t) from min/max
- Average A(z,t) over bubble region to get A(t)
- Untracked A(t) is about ½ nominal value due to mass diffusion; (incompressible) tracked A(t) is virtually constant
- If A(t) is used in definition of alpha, all low compressible simulations agree (with each other, with experiment, with theory)
- If A(t) is used in compressible simulations, all simulations are self similar, but self similar growth rate depends on compressibility



# **Physical Non-Ideal Effects**

- Viscosity, mass diffusion, surface tension
- Compressibility
  - Solution depends on initial temperature stratification; assume isothermal. Initial density depends on height z, so that Atwood number is z dependent.
  - Data interpretation using a time dependent Atwood number restores self similarity, but the mixing rate alpha increases with compressibility.



## Turbulent Mixing: Predictions of Gross Features (Mixing Rate alpha, etc.)

- Systematic agreement of theory, simulation and experiment for RT turbulent mixing
  - Scale breaking physics important to this agreement
- Tracking is the best of practical interface methods
  - Control over numerical mass diffusion and numerical surface tension needed for RT agreement
- Validation studies still in progress (viscosity)



# Other Applications of Front Tracking



## Ask not what the earth can do for us, ask what we can do for the earth



American consumes about 200 billion gallons per year, a 10% saving will be 20 billion gallon amounts to more than 40 billion dollars, not to mention the benefit to the environment.



## **3D Simulation of a Real Fuel Injection**

All parameters are from an experiment performed by Parker\*

nozzle radius (R) grid fuel density gas density fluid viscosity surface tension

0.1mm 20/R 0.66 g/cm<sup>3</sup> 0.0165 g/cm<sup>3</sup> 0.013 Poise 24 mN/m<sup>2</sup>

Reynolds number20,300Weber number $2.2 \times 10^6$ Ohnesorge number0.073Density ratio40





## Verification: Rayleigh Instability

Comparison with the dispersion relation



#### The relative errors of the growth rate

Number of cells on radius	FT/GF M (2D)	FT/GFM (3D)
5	0.1396	0.2853
10	0.0607	0.1702
20	0.0321	0.0672

dispersion relation

$$\beta^2 = \frac{\sigma k}{\rho a^2} (1 - k^2 a^2) \frac{I_1(ka)}{I_0(ka)}$$

 $\begin{array}{l} \rho \mbox{ liquid density} \\ a \mbox{ jet diameter} \\ I_i \mbox{ modified Bessel functions} \\ \mbox{ of the first kind} \end{array}$ 

 $\begin{array}{l} k \mbox{ wave number} \\ \sigma \mbox{ surface tension coefficient} \\ \beta \mbox{ growth rate} \end{array}$ 

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**Incompressible fluid equation** 

# $\mathbf{u}_{\mathbf{t}} + (\mathbf{u}\nabla\cdot\mathbf{u}) = -\nabla p + \nu\nabla^{2}\mathbf{u}$ $\nabla\cdot\mathbf{u} = \mathbf{0}$

This is a mixed hyperbolic and elliptic equation

U is the velocity of fluid and p is the pressure.



## Incompressible Rayleigh-Taylor instability on Reynold number (from left: 14,140,1400)



### **Incompressible code in 3D**



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## **Iwo Dimensional Solute Precipitation**



user: zhaoyh Sun Sep 28 15:35:44 2008



## **Three Dimensional Solute Precipitation**





## Dissolution is the opposite process of

deposition

#### Mesh **60** DB: 2d-Intfc.vtk Cycle: 42703 Time:27 Var: mesh Pseudocolor 50 DB: liquid.vtk Var: concentration -0.7500 40 - 0.5000 -0.2500 30 — 0.000 Max: 1.000 Min: 0.000 **Y-Axis** 20 10 -0 -10-1 1 -10 0 10 20 30 40 50 60 X-Axis



# The Spring Model for two dimensional surface





user: jdkim Fri Jun 3 11:01:34 2011

user: jdkim Tue May 17 11:29:29 2011



## The X Parachute







#### X マフ

SciDA



**Fluid-Rigid body interaction** 





Simulation of Cell Migration







## American and other exotic options

The Black-Schole Equation:

$$\frac{\partial C}{\partial \tau} - \gamma S \frac{\partial C}{\partial S} - \frac{1}{2} \sigma^2 S^2 \frac{\partial^2 C}{\partial^2 S} + (\gamma - D)C = 0,$$
  
$$\tau = T - t$$

Initial Condition:

The interface Condition at all time:  $C(S,0) = 0, \qquad S \le E$  $C(S,0) = S - E, \qquad S > E$ 

$$C_f = \left(S - E\right)$$
$$\frac{\partial C_f}{\partial S} = 1$$

American and many other exotic options are PDE free boundary problems. Front tracking provides an accurate tool to solve the basket hedging problems. We have already established 1-D and 2-D computational platform for such problems.



## One Dimensional American options



## Front tracking on 1-D American call option

## Front tracking on 1-D American put option



## World's fastest computers (top 500)



From mega scale, peta scale, to exa sacle



# **Tarallelization of Front Tracking**





## Parallel load balancing



Like AMR, FronTier has encountered great obstacle in load balancing and parallel scaling. One important development is adaptive partition load balancing.Up to 8196 processors have been tested. No better for number larger than that.



## Parallel Performance of FT

#### Performance of LGB

- Jet simulation
- 300-3million Triangles
- Bluegene/L 4096 cores



#### Weak scaling

- Rayleigh Instability
- Bluegene/L

Grid	Partition	nCores	Time to solution(s)	Ideal(s)
256×256×128	16×16×8	2048	157.1	157.1
256×256×256	16×16×16	4096	157.5	157.1
256×256×512	16×16×32	8192	158.2	157.1
256×256×1024	16×16×64	16384	159.8	157.1



## A quotation from Albert Einstein

"Computers are incredibly fast, accurate, and stupid;

humans are incredibly slow, inaccurate, and brilliant;

together they are powerful beyond imagination."

**Albert Einstein** 

## Major Computing Resources:

- 1. Stony Brook, AMS Department, galaxy cluster (over 500 processors)
- 2. Stony Brook, CEAS, Seawulf cluster
- 3. New York Blue: 103.22 teraflops

WERFULBEYOND MAGINATION

## Thank you for your attention



